



BASIC FORMULAS

H= Head(m)

Q = Flow(m³/h)

Eff = Pump Eff%

Density = SG

Capacity

$$l/sec \times 3.6 = m^3/h$$

$$m^3/h \div 3.6 = l/sec$$

$$Imp\ gpm \times 0.2271 = m^3/h \quad m^3/h \times 4.403 = Imp\ gpm$$

$$US\ gpm \div 0.246 = l/min \quad l/min \times 0.246 = US\ gpm$$

$$10000\ kg/hr = \frac{10m^3h}{Density(SG)}$$

Head/Pressure

$$Ft \div 3.28 = m$$

$$m \times 3.28048 = Ft$$

$$Bar \times 100 = kpa$$

$$m \times 9.805 = kpa$$

$$kpa \times 0.102 = m$$

$$m \times 0.098 = Bar$$

$$Bar \times 10.19 = m$$

$$m \times 1.45 = psi$$

$$psi \times 6.895 = kpa$$

Power

$$hp \times 0.746 = kw$$

$$kw \times 1.340483 = hp$$

$$kw\ abs = \frac{Q \times H \times SG}{367 \times Eff(\%)}$$

$$kw = \frac{Amps \times Volts \times Power\ Factor \times 1.732}{1000}$$

$$RPM = \frac{Hz \times 120}{No\ of\ Poles}$$

$$Hz = \frac{RPM \times No\ Of\ Poles}{120}$$

$$Velocity\ m/sec = \frac{Q \times 353.63}{(Pipe\ Dia)^2}$$

Efficiency

$$EFF(\%) = \frac{Q \times H \times SG}{367 \times kw(abs)}$$

Temperature

$$Deg.C = (deg.F-32) \times 0.556$$

$$Deg.F = (1.8 \times deg.C) + 32$$

Peripheral Speed

$$Peripheral\ Speed(Impeller) = \frac{imp.dia.(mm) \times \pi \times N(Rpm)}{60 \times 1000}$$

Viscosity

vis Viscous Liquid

w Water

Given: Qvis in m³/h kinematic viscosity v in mm²/s

Hvis in m pvis in kg/dm³

$$Qw = \frac{Qvis}{CQ}$$

$$Hw = \frac{Hvis}{CH}$$

$$Qw = C\% \times \%w$$

$$Pvis = \frac{Qvis \times Hvis \times Pvis}{367 \times Eff(\%) \times vis}$$

Centrifugal and Axial Flow Pump Affinity Laws:

Speed changes & impeller diameter remains the same:

$$Q1/Q2 = N1/N2$$

$$H1/H2 = (N1/N2)^2$$

$$P1/P2 = (N1/N2)^3$$

Impeller diameter changes and speed remains the same:

$$Q1/Q2 = D1/D2$$

$$H1/H2 = (D1/D2)^2$$

$$P1/P2 = (D1/D2)^3$$